



## RESEARCH ARTICLE

# Preparation of large, ultra-flexible and free-standing nanomembranes of metal oxide–polymer composite and their gas permeation properties

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## Abstract

In this work, fabrication of free-standing nanomembranes of metal oxide ( $\text{MO}_x$ ) and polymers by simple spin-coating method is discussed. First, double-layer nanomembranes containing  $\text{MO}_x$  and epoxy resin of polyethyleneimine and poly[(*o*-cresyl glycidyl ether)-co-formaldehyde] were prepared. Free-standing nanomembranes were successfully prepared, but defects formed in the metal oxide nanolayer during sharp bending of the nanomembrane. To overcome fragility of  $\text{MO}_x$  nanolayer, poly(vinyl alcohol) nanolayers were introduced between  $\text{MO}_x$  nanolayers by layer-by-layer (LbL) assembly process. The LbL nanomembrane was also free-standing and was highly flexible during macroscopic membrane manipulations. Even after transfer of the LbL nanomembrane onto a porous support, it did not have apparent cracks, confirmed by scanning electron microscopy (SEM). The LbL nanomembrane sustained low gas permeance, confirming the absence of significant defects, although it shows excellent flexibility. We believe that the presented LbL nanomembrane could be a platform useful for the design of molecular nanochannels, which is the next challenge for efficient gas separation.

**Key words:** nanomembranes; free-standing film; ultrathin film; layer-by-layer assembly; metal oxide; gas permeation

## Introduction

Membranes have been explored as an efficient alternative for gas separation over other  $\text{CO}_2$  capture processes, such as liquid absorption and solid adsorption, due to their lower operational energy cost [1, 2]. Organic polymeric membranes have been widely investigated to take advantage of their flexibility and solution processability [3]. However,

such materials are prone to gas permeability–selectivity trade-off behavior [4, 5]. Membranes with high gas flux are strongly sought after although the gas selectivity by the current state-of-the-art membranes is satisfactory for practical use. Thinning is one of the promising approaches to improve the gas permeance of separation membranes. In biological systems, we can find molecularly thin membrane

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and the lipid bilayer membrane. The lipid membrane possesses the fundamental functions as a separating system. Lipid bilayer membrane itself divides the inside and outside of a cell and has a principally barrier property for controlled molecular transport. Transmembrane proteins, such as ion transport proteins, play the main role in the transport of molecules and ions selectively. From this viewpoint, one could say that a lipid bilayer acts both as a barrier membrane and as a platform to deploy such channel proteins for energy-efficient and selective transport. By taking this essential design concept of the biological system, a less permeable membrane with nanometer thickness (nanomembrane) would be considered as a good platform useful for creating molecular channels across this nanomembrane. This is our motivation and starting point to design separation membrane with nanometer thickness.

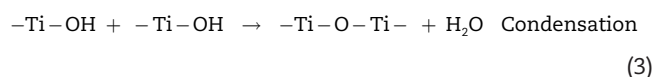
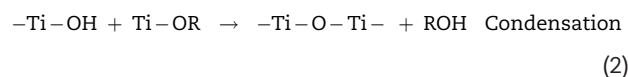
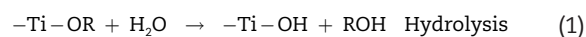
Simple thinning often leads to membrane weakening. In polymeric membranes, fractional free volume plays an important role on molecular permeation across the membranes and, thus, controlling it is one of the issues in membrane design [5]. However, when membranes become thin, the surface property of polymers becomes different from the bulk property. For example, the surface portion of polymer films possesses lower glass transition temperature ( $T_g$ ) because of the localization of its polymer chain and end groups at the surface [6–8]. This different dynamic behavior of the polymer chains near the surface may not allow the design of separation nanomembranes by simply extrapolating from the bulk properties of the polymeric membrane materials.

In contrast, metal oxide materials, such as ceramics and zeolites, have rigid molecular frameworks and, thus, one can design the size and shape of obviously-opened micropores, although the free volume spaces in polymeric membrane can be considered as a temporary pore. This rigid molecular network provides opportunities to more precisely tune molecular transport properties. For example, molecular networks in amorphous ceramic membranes can be designed by the molecular imprinting approach [9–12]. Previously, we demonstrated the facile fabrication of self-supporting ultrathin metal oxide ( $MO_x$ ) films by spin coating and successfully introducing molecular channels via molecular imprinting [9]. Although selective filtration of small organic compounds dissolved in a solvent was tested, the membranes were molecular shape and size selective, which was derived from connected cavities formed during molecular imprinting. However, pure inorganic membranes are highly fragile and become more susceptible to defects when prepared in nanometer thickness. Therefore, improvement in their mechanical property remains a serious problem [3, 10].

Combining the flexibility of organic polymers and the rigidity of molecular network in inorganic materials will provide an alternative method to develop membranes and offer distinct properties different from simply adding together of original polymers and inorganics [10]. Thus,

composite materials are promising for the fabrication of mechanically strong, free-standing, ultrathin membranes with the possibility to tune the molecular transport across the membrane. In addition to mechanical property, incorporation of rigid inorganic structures into the polymer matrix increases  $T_g$  [13–15], which may influence the gas transport in the composite membranes.

Various approaches, such as solution blending [16], casting [17] and layer-by-layer (LbL) assembly, have been investigated for the fabrication of composite nanomembranes [18–22]. Interest in LbL assembly has grown in the last two decades because of its simplicity, ability to control film thickness with molecular scale precision and versatility for many choices of materials architecture. Stepwise surface sol-gel fabrication of metal oxide thin films was introduced independently by Kunitake and co-workers [18] and Kleinfeld and Ferguson [21]. This is a suitable technique for the fabrication of ultrathin composite films by alternate chemisorption of molecular layers of metal oxides and polymers [19, 20]. The chemical reactions during sol-gel processing can be generally described by the following three equations [23].



As we described, a free-standing nanomembrane without severe gas leaking could become a basic platform as a membrane matrix and allow for the design and incorporation of molecular channels across the nanomembrane. With this purpose, we herein report the fabrication of stable and free-standing composite nanomembrane with low gas permeability. Although polymer-inorganic composite films have been investigated by ourselves [10, 24] and other researchers [25], the present nanomembranes are both free-standing and ultrathin. Despite its ultrathinness, the prepared composite nanomembrane showed superior mechanical flexibility. To the best of our knowledge on gas permeance properties, using such composite and free-standing nanomembranes has not been studied previously.

Two approaches for membrane preparation were investigated: surface sol-gel deposition of thin metal oxide films on a free-standing polymer nanomembrane and spin-assisted LbL assembly of alternate polymer and metal oxide layers to form double and molecular multilayers of ceramic-polymer composite nanomembranes. The LbL fabrication method was aimed to improve mechanical stability as a free-standing nanomembrane. The gas permeance properties of the fabricated nanomembranes were also tested.

## 1 Materials and methods

### 1.1 Materials

Silicon wafer with a 350- $\mu\text{m}$  thickness and glass substrate were used for thin-film deposition. Poly(4-vinylphenol) (PVP,  $M_w = 11000$ , Sigma-Aldrich) and polystyrene sulfonate sodium salt (PSS,  $M_w = 70000$ , Polysciences, Inc.) were used as sacrificial layers. Poly(vinyl alcohol) (PVA,  $M_w = 78000$ , 88 mol% hydrolyzed, Polysciences, Inc.), poly[(*o*-cresyl glycidyl ether)-co-formaldehyde] (PCGF,  $M_w = 2500$ , Sigma-Aldrich) and branched polyethyleneimine (PEI,  $M_w = 25000$ , Sigma-Aldrich) were used as polymer layer precursors. Titanium *n*-butoxide (TBO, Sigma-Aldrich and Gelest Inc.), zirconium *n*-butoxide (ZBO, Kanto Chemical), aluminum *s*-butoxide (Gelest Inc.) and tetraethoxy silane (TEOS, Kanto Chemical) were used as metal oxide layer precursors. Ethanol (anhydrous, EMSURE, Germany), *n*-butanol, chloroform and toluene (Wako Ltd.) were used as received. All the chemicals were of analytical grade. Deionized water (18.3 M $\Omega$  cm<sup>-1</sup>, Millipore, Direct-QTM) was used for washing substrate and solution preparation.

### 1.2 Definition of important terms

To avoid confusion with terminology, the following terms are defined:

- Membrane: a film prepared in this work that does not include the porous support.
- Free-standing nanomembrane: a nanometer-thick membrane with self-supporting property, which is

capable of physically sustaining its own membrane shape without porous support.

- Porous support: a highly gas permeable physical support on to which free-standing nanomembrane is placed for a gas permeance experiment.
- Double-layer nanomembrane: a membrane that consisted of  $\text{MO}_x$  layers coated on to a polymer layer.
- Layer-by-layer (LbL) nanomembrane: a membrane comprising multiple LbL coating of  $\text{MO}_x$ -polymer.

### 1.3 Membrane preparation

We herein report two types of free-standing and ultrathin composite nanomembranes of metal oxide and polymers prepared by spin-coating process. Fig. 1 shows the schematic illustrations of each process.

#### 1.3.1 Double-layer nanomembranes of metal oxide and polymer

To fabricate double-layer nanomembranes, we used PEI@PCGF nanomembranes as the underlayer to support  $\text{MO}_x$  layers because PCGF/PEI nanomembranes have sufficient mechanical stability to support its membrane structure without any support (Fig. 1A) [26]. Thus, the PEI@PCGF nanomembrane was firstly prepared followed by a metal oxide deposition to form double-layer nanomembranes.

#### (a) Polymer nanolayer

In this study, glass substrates or silicon wafers were first washed in ethanol, dried by air blowing and treated with

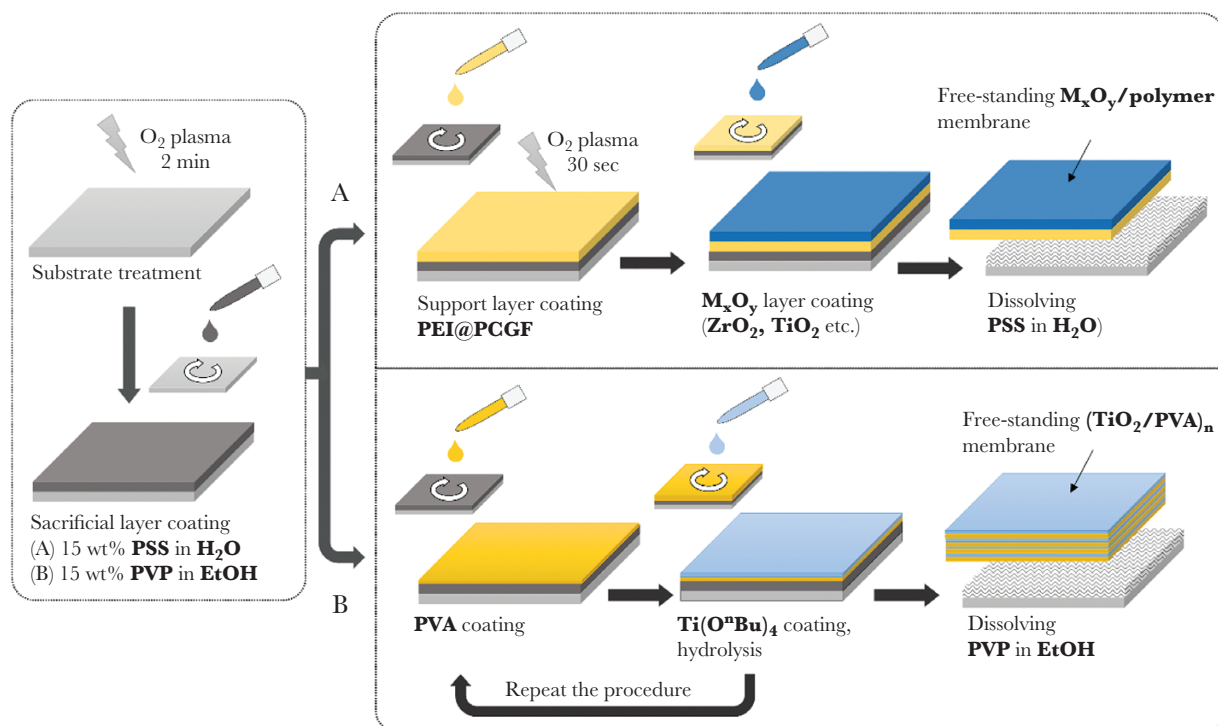


Fig. 1 The schematic representation of nanomembranes fabrication by spin-coating: deposition of  $\text{MO}_x$  layer on polymeric support (A), LbL assembly of  $(\text{PVA}/\text{TiO}_2)_n$  ultrathin membrane (B)

oxygen plasma for 2 min (FA-1, SAMCO, Japan, RF power: 55 W, flow rate of oxygen: 10 sccm, chamber pressure: 20 Pa) to make the substrate surface hydrophilic with the water contact angle (WCA) of  $0.3 \pm 0.1^\circ$ . A 15 wt% aqueous solution of PSS was spin-coated (60 s, 3000 rpm) on the glass substrate and heated at  $120^\circ\text{C}$  for 5 min. The mixture solution of PCGF and PEI (each 1 wt% in chloroform) was separately prepared according to the earlier report [15, 16] and it was coated over the PSS-coated glass by spin coating under the same conditions and heated at  $120^\circ\text{C}$  for 5 min.

#### (b) Metal oxide layer and film detachment

Prior to deposition of the metal oxide layer, the surface of PEI@PCGF on the substrates was treated by  $\text{O}_2$  plasma for 30 s. The water contact angle of the PEI@PCGF layer changed from  $83 \pm 2^\circ$  to  $29.6 \pm 3.9^\circ$ . This plasma treatment is necessary for proper wetting by the next solution coating. Metal oxide sols were separately prepared by first dissolving corresponding metal alkoxides in 1-BuOH to obtain a 100-mM solution. Then a certain amount of 1 M HCl solution was added in the same bottle to achieve 400 mM of water which is necessary for hydrolysis of metal alkoxides. The solution was stirred for 2 h before coating. The metal oxide sols were then spin coated (60 s, 3000 rpm) on the polymer layer surface and then maintained in ambient atmosphere for at least 12 h. Free-standing and double-layer nanomembrane of  $\text{MO}_x$ -polymer were detached from the substrate by immersing the substrate in  $\text{H}_2\text{O}$  to dissolve the PSS sacrificial layer. For the gas permeance test, the membranes were transferred onto track-etched polycarbonate support (see Supplementary video S1 demonstrating detachment and transfer processes).

#### 1.3.2 Molecularly layered nanomembranes of $\text{TiO}_2$ and PVA

A PVP layer was first deposited on a glass substrate by spin-coating (60 s, 3000 rpm) of PVP-ethanol solution (15 wt%) and aqueous PVA (0.3 wt %) was then deposited on this substrate by spin coating (2 min, 3000 rpm) (Fig. 1B). The PVA layer was allowed to dry in ambient air for 1 h. This PVA deposition introduces hydroxyl groups on the substrate and results in the formation of a well-cross-linked network of metal oxide [5]. Then, a TBO solution (50 mM, in toluene) was spin coated (2 min, 3000 rpm) and left in an ambient air for 30 min to undergo hydrolysis and condensation. This alternate sol-gel deposition cycle of PVA and  $\text{TiO}_2$  was repeated until the desired film thickness was reached. Film growth on a quartz plate during this repetitive process was monitored by UV/Vis spectrophotometer (Jasco V-670). After dissolving the sacrificial layer of PVP in ethanol, the detached film was freely floating on an ethanol solution. It was then transferred onto an anodized porous alumina support (Anodisc, G.E. Healthcare) for surface observation and gas permeation tests.

Film thickness and surface morphology were observed using an optical microscope (Keyence VHX-600) and a field emission scanning electron microscope (FE-SEM, Hitachi S-5200).

## 1.4 Gas permeation experiment

Gas permeation properties of nanomembranes on a porous support were measured using a commercial instrument (GTR-11A/31A system, GTR Tec Corp., Japan) coupled to gas chromatography, as described in more details elsewhere [24]. Once the nanomembranes were prepared and transferred onto a porous support, the membrane area was fixed by Kapton and/or alumina tapes with an open hole of 1 cm diameter as shown in Fig. 2A.

Fig. 2B shows the experimental gas permeation setup. Pure and mixed gases were introduced to the feed side of the membrane cell at room temperature. The pressure of the feed gas was set at 100 kPa as a gauge pressure while the permeate side was maintained in a vacuum condition, giving a total pressure difference of ca. 200 kPa. The volume of gas passed through the membrane per unit time was measured. Gas permeance was then calculated from the measured volume.

Permeance of the gas ( $P$ ) and separation factor ( $\alpha$ ) were determined according to the following equations:

$$P = N / (A \cdot \Delta P)$$

$$\alpha = P_{\text{CO}_2} / P_{\text{N}_2}$$

where  $N$  (in  $\text{m}^3/\text{s}$ ),  $A$  (in  $\text{m}^2$ ) and  $\Delta P$  (in Pa) are the flow rate measured on the permeation side, effective membrane area and pressure difference, respectively. In this experiment, effective area ( $A$ ) for gas permeation was  $0.785 \text{ cm}^2$  (1 cm membrane diameter). For easier comparison, the permeance was reflected in the common GPU unit, where  $1 \text{ GPU} = 7.5 \times 10^{-12} \text{ m}^3/(\text{m}^2 \text{ s Pa})$ .

## 2 Results and discussion

### 2.1 Double-layered nanomembranes of metal oxide and polymer

In the first trial, we have attempted to form the stable thin metal oxide layers deposited on well-established polymeric nanomembrane [27]. Fig. 3 shows the variety of metal oxide layers on PEI@PCGF. The deposition of the  $\text{MO}_x$  layer significantly reduced the macroscopic flexibility of the membrane. Thin polymeric membranes with the thickness of less than a few hundred nanometers are usually difficult to manipulate. However, the presence of the oxide layer makes the membrane stretch easily on (or in) the solvent (Fig. 3A) after the dissolution of the sacrificial layer. Due to this improved strength, it was quite easy to place such a double-layer nanomembrane on the metal frame as shown in Fig. 3B. Figs. 3C–E and G shows the cross sections of double-layer nanomembranes transferred onto a silicon wafer. In all cases, the formation of the thin and uniform double layers was clearly observed. Film thickness of the different



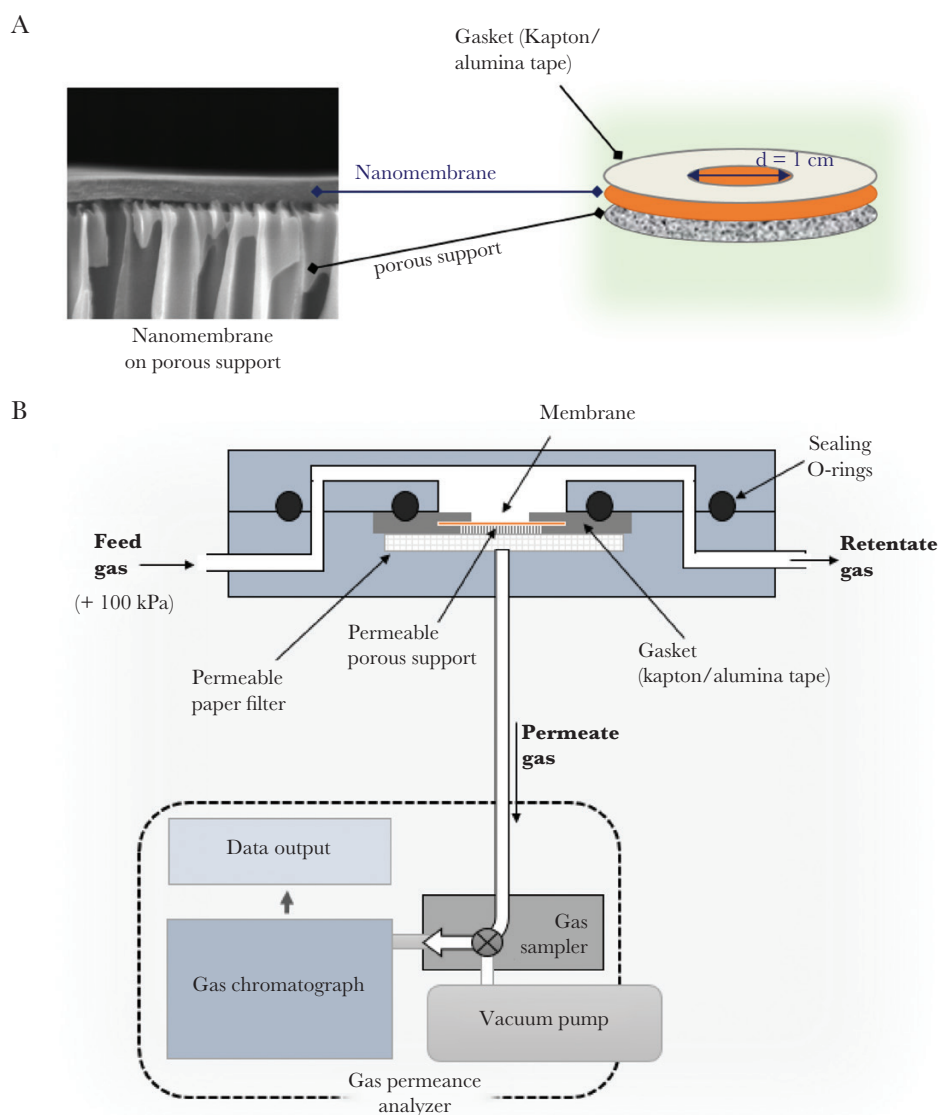
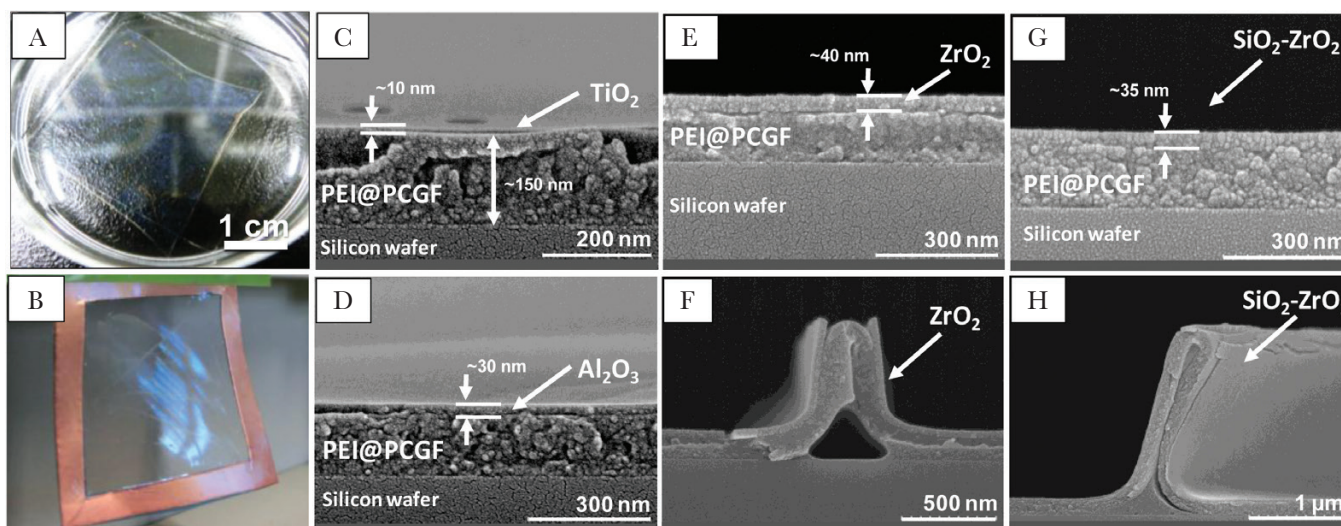


Fig. 2 A schematic representation of (A) nanomembrane assembly for gas permeation experiment and (B) gas permeance measurement apparatus

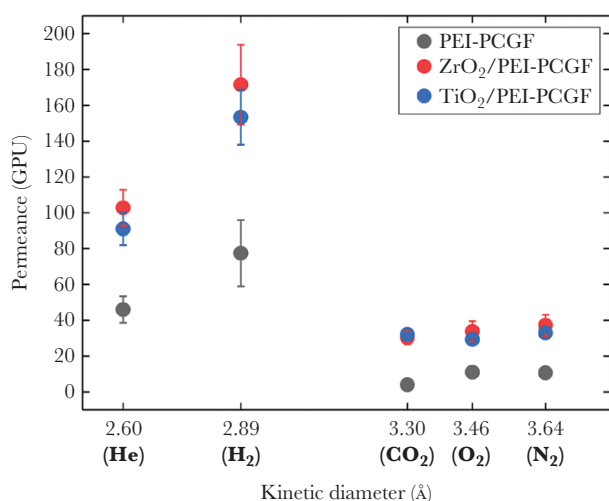
$MO_x$  varied from 10 to 40 nm, and the thickness of polymer layer was ca. 150 nm. Sharply bent nanomembranes shown in Fig. 3C and G demonstrated that thin metal oxide (ceramic) layer could not follow the flexible bending of the PEI@PCGF layer. However, it is evident that different oxides showed different flexibility. It can be seen that the  $ZrO_2$  layer on PEI@PCGF undergoes more damage upon membrane bending compared with mixed oxide layer  $ZrO_2:SiO_2 = 1:1$  (Fig. 3F and H, respectively). Although the mechanical properties of the double-layer nanomembranes can also be affected by the thickness of the metal oxide layer significantly, this finding may provide a way to improve and adjust the mechanical flexibility of oxide layers.

Five different gases ( $He$ ,  $H_2$ ,  $CO_2$ ,  $N_2$  and  $O_2$ ) were used for testing the gas permeance properties of this double-layer nanomembrane. The PEI@PCGF nanomembrane with the thickness of 150 nm was chosen as a reference. Fig. 4 shows the permeance of gases relatively to their kinetic diameter.

As can be seen, all membranes indeed demonstrate the selectivity towards smaller gases (helium and hydrogen) compared with gases of larger molecular sizes ( $CO_2$ ,  $O_2$  and  $N_2$ ). However, the deposition of metal oxide layer resulted in increased permeance for the double-layer membrane compared with the PEI@PCGF membrane alone. Such permeance increase may be explained by the effect of oxygen plasma treatment and the solvent influence (*n*-butanol) on the polymeric layer during the spin-coating of metal oxide solution. This result is different from earlier reported deposition of  $TiO_2$  nanolayer on PDMS (with thickness  $\sim 1 \mu m$ ) where the decrease in the permeance of composite membrane was observed [24]. Most likely the observed difference may be attributed to the intrinsic properties of polymer support, i.e. PDMS is a highly permeable material while PEI@PCGF has ca. 3 orders lower permeability for  $CO_2$  or  $N_2$ , and short treatment by 1-butanol has slightly changed the polymer matrix. An additional finding from the gas permeance



**Fig. 3** Spin-coated metal oxide layers on the polymer. (A) Digital photo showing the  $\text{TiO}_2/\text{PEI@PCGF}$  membrane detached from the glass substrate freely floating on water; (B) digital photo of the composite membrane having mixed  $\text{SiO}_2$  and  $\text{ZrO}_2$  deposited on the  $\text{PEI@PCGF}$  membrane supported by metal frame; SEM images of the cross section of different metal oxide layers was deposited on  $\text{PEI@PCGF}$  membrane; (C)  $\text{TiO}_2/\text{PCGF@PEI}$ ; (D)  $\text{Al}_2\text{O}_3/\text{PCGF@PEI}$ ; (E)  $\text{ZrO}_2/\text{PCGF@PEI}$ , (G)  $\text{SiO}_2\text{-ZrO}_2/\text{PCGF@PEI}$ ; (F) and (H) the bent places of the  $\text{ZrO}_2/\text{PEI@PCGF}$  and  $\text{SiO}_2\text{-ZrO}_2/\text{PEI@PCGF}$ , respectively, demonstrating that different oxides (or their mixes) provide different flexibility to the film



**Fig. 4** Permeance of gases with different kinetic diameter through the double-layer  $\text{ZrO}_2/\text{PEI@PCGF}$  and  $\text{TiO}_2/\text{PEI@PCGF}$  nanomembranes compared with the supporting  $\text{PEI@PCGF}$  nanomembrane

data is that there is no significant difference between  $\text{TiO}_2$  and  $\text{ZrO}_2$  layers on the permeance or selectivity. Obviously, the chemical nature of the oxide material is quite simple and no specific interaction with gases is expected. Although the separation of different gas pairs is not extraordinary, here we demonstrate the way to assemble metal oxide films supported by organic nanomembrane. By considering the results of scanning electron microscopy (SEM), the double-layer nanomembranes may have defects even with careful manipulation of the membranes for transfer on to the porous supports. The defects may be few and insignificant because the gas permeance was not changed drastically. Despite potential defects, we believe that the usage of this membrane architecture is not completely disadvantageous.

In particular, the metal oxide layer, in contrast to polymer, may work as a suitable matrix for small molecules incorporation. For example, in our previous work [24], we showed that addition of  $\text{CO}_2$ -philic component (phthalic acid) into the metal oxide layer allowed improving the selectivity toward  $\text{CO}_2$  separation from  $\text{CO}_2/\text{N}_2$  mixture.

## 2.2 LbL Nanomembranes

Defects were observed on the double-layer nanomembranes of  $\text{MO}_x$  and  $\text{PEI@PCGF}$  (Fig. 3F and H). This is due to the layers of the polymer and  $\text{MO}_x$  existing in the membrane separately, which results in an obvious ceramic nature of the  $\text{MO}_x$  layer. To overcome this fragility problem, we tried to fuse them at a molecular level by a sequential spin coating of the thin layers of the polymer and  $\text{TiO}_2$  using the surface sol-gel process. In this case, PVA was employed as a polymer layer; since PVA has a lot of hydroxyl group at the side chain, which can react with metal alkoxides through sol-gel reaction.

UV-Vis absorbance spectra for five cycles of PVA/ $\text{TiO}_2$  deposition is shown in Fig. 5A. The linear absorbance increases of  $\text{TiO}_2$  at 252 nm against the cycles of deposition implied that the  $\text{TiO}_2$  layer of similar thickness was deposited at each cycle (Fig. 5B). The UV-Vis observation was unable to track the deposition of PVA; however, earlier works suggested that PVA is readily anchored to the titanium alkoxides due to the abundance of hydroxyl groups on its surface [28].

A highly flexible and free-standing membrane was successfully prepared after dissolving the sacrificial layer and was transferred onto a porous support. Fig. 6A demonstrates the aspiration process of a centimeter-scale membrane into a micropipette with a 2-mm diameter hole. The

detached membrane, which was floating in ethanol, was aspirated into the micropipette and released back to the solvent. The membrane undergoes multiple bending to fit the mouth of the micropipette during the sucking/release process. Once released into the solvent, the film regained its original shape and size through a simple assistance by spatula (see Supplementary video S2).

The SEM investigation showed that the fabricated nanomembrane has a smooth and uniform surface; large defects were not observed even after macroscopic manipulation. Fig. 6C and D shows the top and cross-sectional

views of a 60-nm thick free-standing membrane prepared by an alternate coating of PVA and TiO<sub>2</sub> for 6.5 cycles (13 alternate layers), transferred onto an Anodisc. Thickness was uniform throughout the membrane. For the observed thickness, the average thickness for one cycle deposition of PVA and TiO<sub>2</sub> is calculated to be about 10 nm. Although layered morphologies were vaguely seen in the membrane cross section (Fig. 6D), no interspace between layers was observed, suggesting that each layer was well adhered. This result should be due to the result of interfacial sol-gel reaction between the hydroxyl groups of PVA and Ti(O<sup>n</sup>Bu)<sub>4</sub>.

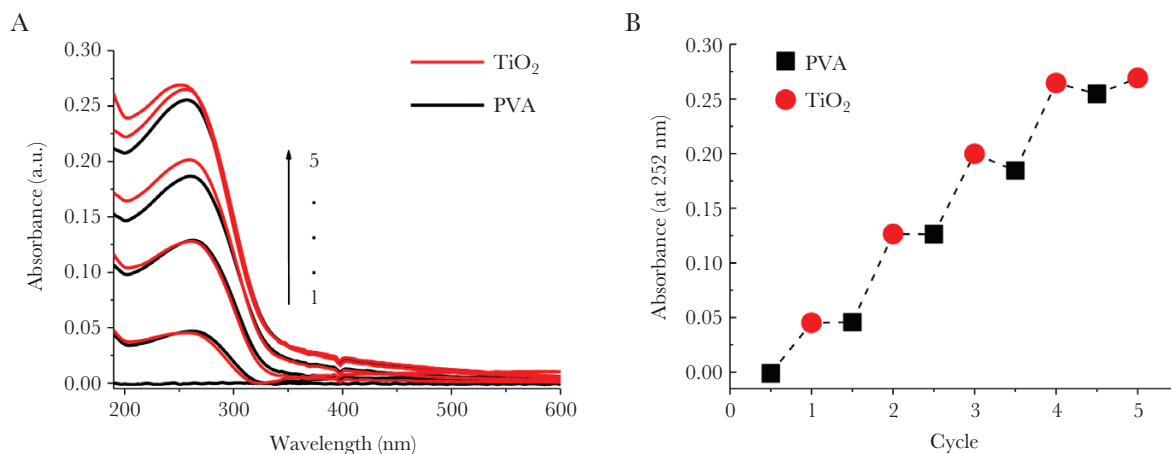


Fig. 5 (A) UV/Vis absorption spectra of sequential PVA/TiO<sub>2</sub> deposition, (B) UV/Vis absorbance at 252 nm of consecutive PVA and TiO<sub>2</sub> layers

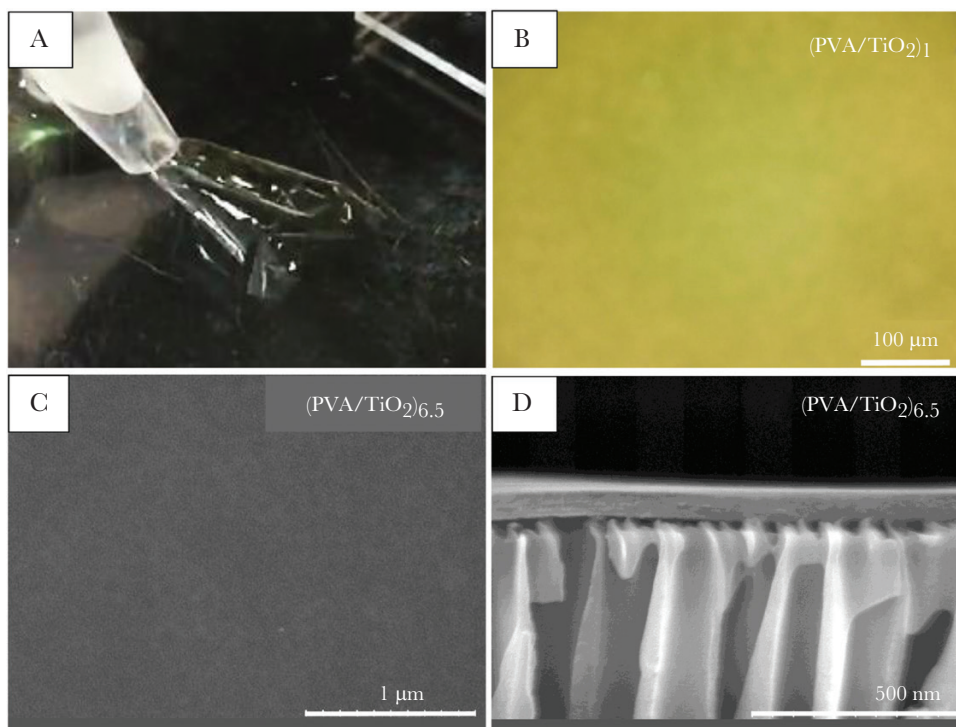


Fig. 6 LbL assembled (PVA/TiO<sub>2</sub>)<sub>n</sub> composite nanomembrane. (A) Digital photograph showing the aspiration process of the freestanding centimeter-scale (PVA/TiO<sub>2</sub>)<sub>6.5</sub> nanomembrane into a micropipette; (B) optical microscope image of the surface bi-layer PVA/TiO<sub>2</sub> film deposited on silicon wafer; (C) surface and (D) cross-sectional view FE-SEM images of the free-standing (PVA/TiO<sub>2</sub>)<sub>6.5</sub> nanomembrane transferred onto a porous alumina (Anodisc) support



Molecular flexibility of metal oxides was discussed [29] and their intrinsic molecular flexibility contributed to the observed excellent flexibility in macroscopic scale as seen in the aspirating experiment of the LbL nanomembrane.

We could detach the LbL nanomembrane that consisted of as low as three cycles (ca. 30 nm), and successfully transferred it onto a porous support without any significant damage. Thus, incorporation of polymer network into the ceramic molecular layers by LbL assembly method, in contrast to double-layer  $\text{MO}_x$ -polymer structures, played an important role for the significant improvement of film mechanical flexibility and surface smoothness.

Gas permeation of the LbL nanomembrane with the thickness of ca. 60 nm was tested by using  $\text{N}_2/\text{CO}_2$  (95:5)

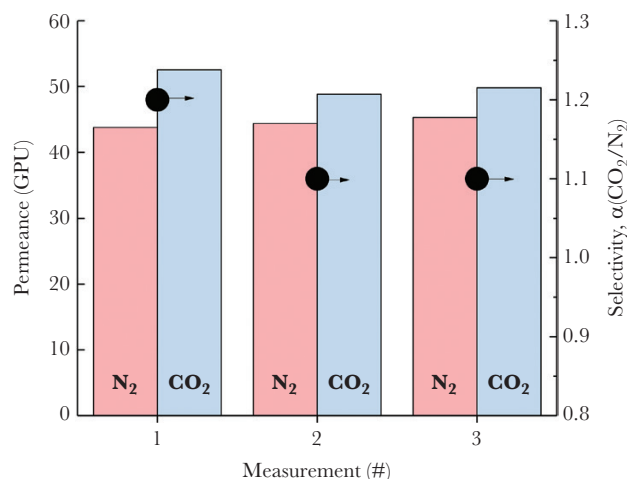


Fig. 7 Gas permeance of PVA/ $\text{TiO}_2$  multilayer nanomembrane

mixture gas. The membranes showed low gas permeance property (Fig. 7).  $\text{TiO}_2$  and PVA themselves are not expected to have preferential interaction with  $\text{CO}_2$  and  $\text{N}_2$ . Thus, we believe that this nonselective gas permeation is reasonable. In support of the SEM data, the observed small gas permeance indicated that there was no significant leakage pathway in the membrane. This LbL nanomembrane would have potential as a basic membrane matrix, which we described in the Introduction section.

### 3 Discussion

Fig. 8 shows the schematic illustration of the double-layer and LbL nanomembranes prepared in this work. Although the gas permeation property of the amorphous metal oxide is currently unknown, the internal structure suggests several future expectations from these nanomembranes.

In the double-layer nanomembrane, the mechanical properties of each polymer and  $\text{MO}_x$  layers may not be fused at the nanometer scale. Thus, the  $\text{MO}_x$  layer showed fragility at the nanometer scale, leading to layer breaking, although the macroscopic flexibility in the LbL membrane was improved. From this viewpoint, a molecularly layered structure in LbL nanomembrane contributes to the fusion nature of polymer and  $\text{MO}_x$  at the molecular scale. An LbL nanomembrane showed low gas permeability, which is several orders smaller compared with conventional gas separation polymer membranes. The pin-hole-free membrane was not prepared and further optimization to prepare nanomembrane with less defects is underway, and will be reported elsewhere. At the same time, the next challenge with these nanomembranes is to incorporate

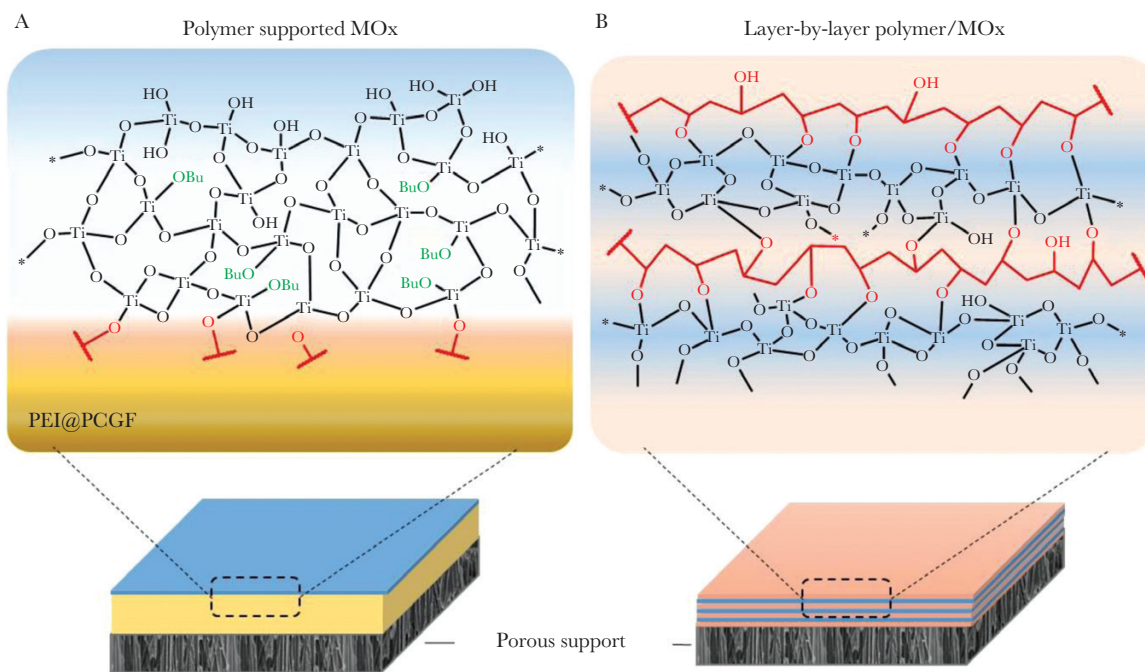


Fig. 8 Schematic representation of the internal chemical structure of metal oxide ( $\text{TiO}_2$ ) layer. (A) Assembled on PEI@PCGF and (B) LbL assembled ( $\text{PVA}/\text{TiO}_2$ )<sub>n</sub> nanomembrane



(or design) nanochannels to transport gas molecules selectively. Metal oxides (in particular,  $\text{TiO}_2$ ) can also be used as matrices for molecular imprinting [11, 12]. The microporosity of amorphous  $\text{TiO}_2$  imprinted by template molecules enabled the formation of selective sites in nanomembranes. Furthermore, we reported that the incorporation of  $\text{CO}_2$ -philic compound (phthalic acid) in the  $\text{TiO}_2$  matrix resulted in significant  $\text{CO}_2/\text{N}_2$  selectivity improvement ( $\alpha \sim 150$ ) [24]. This result encouraged us to design the channel structures in a nanomembrane. For the systematic investigation on the nanochannel design, the features of LbL nanomembrane without high gas selectivity could be useful to distinguish the effect of the design.

In addition, the described membranes may possess an asymmetric structure, i.e. oxide or polymer layer may be facing the gas stream first, leading to anisotropic gas separation property, depending on the feed gas direction. In the case of LbL nanomembranes having the simplest  $(A/B)_n$  structure, where A and B are two different components, we can expect differences in response of  $A/(B/A)_n$  and  $B/(A/B)_n$  architectures. Several projects ongoing in our laboratory are investigating these and other effects of the membrane morphology on gas separation.

Therefore, we believe that amorphous metal oxide films, whether used as layers in composite membranes (once the mechanical properties improved) or as free-standing LbL nanomembranes present an interesting architecture for separation membranes in the future.

## 4 Conclusion

Two types of nanomembranes,  $\text{MO}_x$ -polymer double-layer nanomembrane and LbL assembly of  $\text{TiO}_2$  and PVA, were successfully fabricated by simple spin-coating and tested for gas permeation.

Double-layer nanomembranes ( $\text{MO}_x$ -PEI@PCGF) demonstrated slightly higher permeance for five different gases compared with PEI@PCGF nanomembrane alone, without significant influence on gas selectivity. Faster gas permeation was plausibly induced by plasma treatment and solvent swelling during the oxide layer coating. SEM observation showed that the metal oxide layer cannot follow the flexibility of polymer and develop defects when the membrane is mechanically disturbed.

PVA was introduced between  $\text{MO}_x$  nanolayers by LbL assembly process to overcome fragility of the metal oxide nanolayer. The fabricated nanomembrane was free-standing and showed high flexibility without any film fragmentations during macroscopic membrane manipulations. Even after transfer of LbL nanomembranes onto a porous support, it did not have obvious cracks as confirmed by SEM observation. Nanomembrane sustained low gas permeance, confirming the absence of significant defects, although it shows excellent mechanical property.

Highly flexible and free-standing composite nanomembrane of polymers and metal oxides such as these are expected to provide great opportunities in the design of gas separation membranes as a platform for molecular nanochannel design.

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*Conflict of interest statement.* The authors declare no competing financial interest.

## Supplementary data

Supplementary data is available at *Clean Energy* online.

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